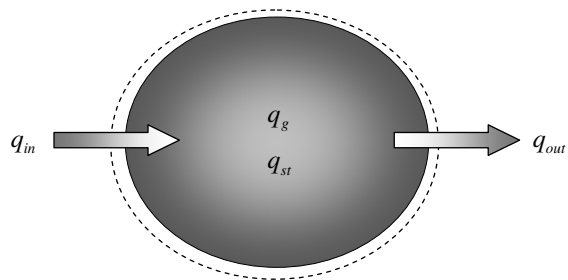


control volume



energy balance:

$$q_{in} - q_{out} + q_g = q_{st}$$

$$V = \text{volume} \quad \left[\frac{m^3}{m^3} \right]$$

$$\rho = \text{density} \quad \left[\frac{kg}{m^3} \right]$$

$$c_p = \text{specific heat} \quad \left[\frac{J}{kg \cdot K} \right]$$

$$k = \text{thermal conductivity} \quad \left[\frac{W}{m \cdot K} \right]$$

$$\alpha = \frac{k}{\rho c_p} \text{ thermal diffusivity} \quad \left[\frac{m^2}{s} \right]$$

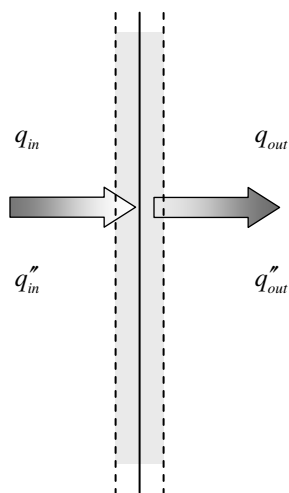
$$q = \text{rate of heat transfer} \quad [W]$$

$$q_g = \dot{q}V \text{ rate of energy generation} \quad [W]$$

$$\dot{q} = \text{volumetric heat source} \quad \left[\frac{W}{m^3} \right]$$

$$q_{st} = \rho c_p \frac{\partial T}{\partial t} V \quad \text{rate of change of energy stored}$$

control surface



energy balance:

$$q_{in} = q_{out}$$

$$q''_{in} = q''_{out}$$

Derivation of q_{st}

$$1^{st} \text{ Law of Thermodynamics} \Rightarrow \Delta Q - W = \Delta U \quad [J]$$

change of internal energy
is caused by heat transferred
to a control volume
during the process

$$\Delta Q = \Delta U$$

incompressible
substance

$$\Delta U = mc_p \Delta T$$

$$\Delta t = \text{time of the process} \quad \frac{\Delta Q}{\Delta t} = mc_p \frac{\Delta T}{\Delta t} \quad \left[\frac{J}{s} \right]$$

$$\text{take } \Delta t \rightarrow 0 \quad \dot{Q} = mc_p \frac{\partial T}{\partial t} \quad [W]$$

$$\text{denote } \dot{Q} \equiv q \quad q = mc_p \frac{\partial T}{\partial t}$$

$$m = \rho V$$

$$q = (\rho V) c_p \frac{\partial T}{\partial t}$$